

WHAT IS CLAIMED IS:

1. A Fischer-Tropsch catalyst for the conversion of synthesis gas into Fischer-Tropsch products, the catalyst comprising:
 - 5 a structured catalyst support;
 - an active metal for promoting a Fischer-Tropsch reaction disposed on the catalyst support; and
 - wherein the support has a voidage ratio greater than 0.6.
- 10 2. The catalyst of Claim 1 wherein the catalyst support has a linear dimension of at least 200 microns.
- 15 3. The catalyst of Claim 1 wherein the catalyst support has a linear dimension of at least 500 microns.
4. The catalyst of Claim 1 wherein the catalyst support has a linear dimension of at least 700 microns.
- 20 5. The catalyst of Claim 1 wherein the catalyst support has a linear dimension of at least one inch.
6. The catalyst of Claim 1 wherein the Fischer-Tropsch catalyst has a catalyst concentration for a given volume of at least 10 percent.
- 25 7. The catalyst of Claim 1 wherein the catalyst support is formed with a mean L/D less than 20.
8. The catalyst of Claim 1 wherein the catalyst is operable to produce a productivity in the range of 200 - 4000 vol CO/vol. catalyst/hour or greater over at least a 600 hour run of a Fischer-Tropsch reactor with the catalyst therein.

9. A Fischer-Tropsch catalyst system for the conversion of synthesis gas into Fischer-Tropsch products, the catalyst system comprising a Fischer-Tropsch catalyst with a voidage ratio greater than or equal to 0.45 and a catalyst concentration for a given volume of at least 10 percent.

10. A method of preparing a Fischer-Tropsch catalyst for use in converting synthesis gas into Fischer-Tropsch products, the method comprising the steps of:

5 providing a structured catalyst support having a voidage ratio greater than 0.6; and applying an active metal for promoting a Fischer-Tropsch reaction to the catalyst support.

10 11. The method of Claim 10 wherein the step of providing a catalyst support comprises providing a catalyst support having a mean L/D ratio of less than 10.

15 12. The method of Claim 10 wherein the step of providing a catalyst support comprises providing a catalyst support having at least one linear dimension greater than 200 microns.

20 13. The method of Claim 10 wherein the step of providing a catalyst support comprises providing a catalyst support having at least one linear dimension greater than 500 microns.

25 14. The method of Claim 10 wherein the step of providing a catalyst support comprises providing a catalyst support having at least one linear dimension greater than 700 microns.

30 15. The method of Claim 10 wherein the step of providing a catalyst support comprises providing a catalyst support having at least one linear dimension greater than one inch.

16. A system for converting CO and H₂ into Fischer-Tropsch products through the Fischer-Tropsch reaction, the system comprising:

- 5 an inlet;
- a reactor fluidly coupled to the inlet for receiving CO and H₂;
- 10 a stationary, structured Fischer-Tropsch catalyst disposed within the reactor for converting at least a portion of the CO and H₂ into Fischer-Tropsch products through Fischer-Tropsch reaction; and
- wherein the structured catalyst has a voidage ratio greater than or equal to 0.6.
- 15 17. The system of Claim 16 wherein the structured Fischer-Tropsch catalyst disposed within the reactor has at least a catalyst concentration of 30 percent.
18. The system of Claim 16 wherein the structured Fischer-Tropsch catalyst has a linear dimension of at least 500 microns.
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19. A system for converting shorter-chain hydrocarbons into longer-chain hydrocarbons, the system comprising:

- 5 a feed stream preparation subsystem for receiving an oxygen-containing gas, light hydrocarbons, water, and tail gas, and preparing the feed streams for conversion to synthesis gas;
- 10 a synthesis-gas subsystem for receiving feed streams of oxygen-containing gas, light hydrocarbons, and steam and preparing therefrom synthesis gas;
- 15 a synthesis subsystem for receiving synthesis gas from the synthesis-gas subsystem and for converting at least a substantial portion of the synthesis gas into longer-chain hydrocarbons through the Fischer-Tropsch reaction; and
- 20 wherein the synthesis subsystem comprises:
- a saturator unit having an inlet for receiving a circulating hydrocarbon liquid and an inlet for receiving synthesis gas, the saturator for substantially saturating a hydrocarbon liquid with synthesis gas introduced into the saturator;
- 25 a reactor fluidly coupled to the saturator unit for receiving a saturated hydrocarbon liquid therefrom; and
- 30 a stationary, structured Fischer-Tropsch catalyst disposed within the reactor for converting at least a portion of a saturated hydrocarbon liquid into longer-chain hydrocarbons.

20. A system for converting synthesis gas into longer-chain hydrocarbon products through the Fischer-Tropsch reaction, the system comprising:

5 a saturator unit having an inlet for receiving a circulating hydrocarbon liquid and an inlet for receiving synthesis gas, the saturator for substantially saturating a hydrocarbon liquid with synthesis gas introduced into the saturator;

10 a reactor fluidly coupled to the saturator unit for receiving a saturated hydrocarbon liquid therefrom; and

15 a stationary, structured Fischer Tropsch catalyst disposed within the reactor for converting at least a portion of a saturated hydrocarbon liquid into longer-chain hydrocarbons through a Fischer-Tropsch reaction.

20 21. The system of Claim 20 further comprising a heat exchanger associated with the reactor for removing heat from the reactor.

22. Method for converting synthesis gas into Fischer-Tropsch products through the Fischer-Tropsch reaction, the method comprising the steps of:
- 5 delivering CO and H₂ to a reactor having a stationary, structured Fischer-Tropsch catalyst disposed in the reactor; and
- 10 causing the CO and H₂ to flow through the reactor whereby the stationary, structured Fischer-Tropsch catalyst converts at least a portion of the CO and H₂ into Fischer-Tropsch products.
15. The method of Claim 22 wherein the step of delivering CO and H₂ to the reactor comprises the steps of: saturating a hydrocarbon liquid with synthesis gas and delivering the saturated hydrocarbon liquid to the reactor.
20. The method of Claim 22 wherein the step of delivering CO and H₂ to the reactor comprises the step of delivering synthesis gas to the reactor.
25. The method of Claim 22 wherein the step of delivering CO and H₂ to the reactor comprises the steps of: saturating a hydrocarbon liquid with synthesis gas, delivering the saturated hydrocarbon liquid to the reactor, and delivering synthesis gas to the reactor.